

Process Name:

Reference Flow:

NETL Life Cycle Inventory Data Process Documentation File

Chromium products

1 kg of chromium product

Brief Description:		roduction of chro hromium metal	omite, high-carbon ferrochro	omium, or					
Section I: Meta Data									
Geographical Covera	age:	Various	Region: Various						
Year Data Best Represents:		2005							
Process Type:		Manufacturing Process (MP)							
		Cradle-to-Gate Process (CG)							
<u>-</u>		No	No						
Completeness:		Individual Relev	Individual Relevant Flows Recorded						
Flows Aggregated in	Data Se	et:							
✓ Process	☑ Energ	y Use	☐ Energy P&D	☐ Material P&D					
Relevant Output Flo	ws Inclu	ıded in Data Se	et:						
Releases to Air:	☑ Greenhouse Gases		☐ Criteria Air	☑ Other					
Releases to Water:	✓ Inorganic		☐ Organic Emissions	☑ Other					
Water Usage:	☑ Water Consumption		☑ Water Demand (throughput)						
Releases to Soil:	☐ Inorganic Releases		☐ Organic Releases	□Other					
Adjustable Process I	Paramet	ers:							
None									
Tracked Input Flows	5:								
Electricity			[Technosphere] E	Electricity					
Water (municipal)			[Technosphere] Treated water						
Water (ground water) Explosives			[Technosphere] Explosives for mining						
Water (municipal) Water (ground water)			[Technosphere] Fuel for operations						



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Heavy fuel oil, combusted Natural gas, combusted

Liquid petroleum gas, combusted

Light fuel oil, combusted

Flocculant Coal

Coke, imported Coke, local

Char Anthracite Silica sand Electrode paste

Thermal energy (MJ)

Soda ash Sulfuric acid Sulfur Aluminum

Tracked Output Flows:

Chromite concentrate

Ferrochromium

Chromium

Tailings, from chromite beneficiation

FeCr slime

Slag

Iron (III) oxide Sodium sulfate Aluminum oxide [Technosphere] Fuel for operations
[Technosphere] Fuel for operations
[Technosphere] Fuel for operations
[Technosphere] Fuel for operations
[Technosphere] Unspecified flocculant
[Technosphere] Unspecified coal
[Technosphere] Imported coal-coke
[Technosphere] Locally sourced coal-

coke

[Technosphere] Char biomass fuel [Technosphere] Unspecified anthracite [Technosphere] Unspecified sand [Technosphere] Unspecified electrode

paste

[Technosphere] Thermal energy from

any fuel source for rotary kiln [Technosphere] Soda ash

[Technosphere] Sulfuric acid – 100% [Technosphere] Elemental sulfur [Technosphere] Un-alloyed aluminum

Reference flow – mineral concentrate

(95% chromite, 44% Cr) Reference flow – High-carbon ferrochromium (56.7% Cr)

Reference flow - Refined chromium

metal (99% Cr)

Mixed water/solids waste Mixed water/solids waste

Solid waste

Potential co-product Potential co-product Potential co-product

Section II: Process Description

Associated Documentation

This unit process is composed of this document and the data sheet (DS) *DS_Stage12345_M_chromium_products_2016.01.xlsx*, which provides additional details regarding relevant calculations, data quality, and references.



Goal and Scope

This unit process provides a summary of relevant input and output flows associated with the production of chromite, high-carbon ferrochromium, or chromium metal. Aggregated processes include underground mining, surface mining, and beneficiation of chromite; open-furnace and closed-furnace smelting for high-carbon ferrochromium production; and aluminothermic process for chromium metal production.

Boundary and Description

Figure 1 provides an overview of the boundary of this unit process. Rectangular boxes represent relevant sub-processes, while trapezoidal boxes indicate upstream data that are outside of the boundary of this unit process. As shown, the upstream emissions from the electricity, sulfuric acid, and other trapezoidal boxes are calculated in another unit process. The methods for calculating these operating activities are described below.

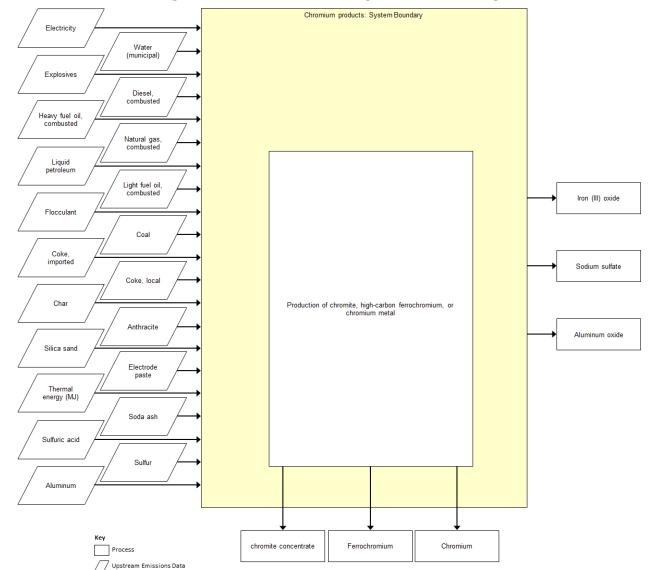


Figure 1: Unit Process Scope and Boundary

This unit process can provide three different products: chromite concentrate, high-carbon ferrochromium, and chromium metal. Chromite is a mineral and the main source of chromium. High-carbon ferrochromium is the primary chromium product globally and is primarily used as an alloying agent in stainless steel. Chromium metal is used in other alloying applications.

This cradle-to-gate unit process aggregates the processes and thus materials and energy necessary to create each of the chromium products. For example chromium metal will include the mining and beneficiation in addition to the processes required to refine chromite into chromium metal.

The data for mining, beneficiation, and smelting came from data compiled for a report sponsored by the International Chromium Development Association (PE International,





2007). Within the report, they detail gate-to-gate inputs, products, and emissions for underground mining, surface mining, beneficiation, and three variations of smelting. All 5 of these gate-to-gate profiles are individually represented in the spreadsheet. When processes need to be connected (e.g., underground mining to beneficiation to openfurnace smelting), they are connected through the parameter scenarios (PS) tab. The philosophy behind this process is that this UP can be used to generate a profile for the different pathways for chromium. The complete system can be modeled externally, and the complete life cycle inventory can be multiplied by the percentages in **Table 1** to provide an average profile. As shown in **Table 1**, the majority of chromite mining is underground, so all of the smelter scenarios (and the chromium metal) are only connected to underground mining.

The production of refining chromium metal was modeled using descriptions of the process and the chemical reactions. The aluminothermic reaction is the modeled process as it represents 95% of the global chromium metal production with electrolytic making up the remainder (USGS, 2011). In preparation for the actual aluminothermic process, chromium (III) oxide is created by first separating the chromium from the iron by roasting the chromite with soda ash in a rotary kiln, creating sodium chromate. This sodium chromate is converted to sodium dichromate by mixing with sulfuric acid, and then the sodium dichromate is calcined with sulfur to yield chromium (III) oxide. The roasting and calcination processes both require heat. It is assumed that the amount of heat required is equal to the activation energy for the specific chemical reactions. While a source for the roasting activation energy could be found, the activation energy for calcining could not be found, so it is assumed to the same as the roasting reaction. Further there will be some efficiency associated with transferring that heat to facilitate the reaction. The efficiency for a rotary kiln was calculated using the activation energy for converting limestone to guicklime (3.16 GJ/Mg) and the average heat input to long dry kilns (5.23 GJ/Mg) giving an efficiency of 60.4%.

Judging from the available material, there is no heat input required for the aluminothermic reaction, as the heat for the reaction initially comes from igniting a mixture of aluminum and barium peroxide which provides the heat necessary to trigger the exothermic reaction reducing Cr_2O_3 to Cr and also Al_2O_3 .



Table 1: Production splits for high-carbon ferrochromium pathway

Processes	Share of production		
Mining			
Underground	82.8%		
Surface	17.2%		
Smelting			
Open furnace	44.4%		
Closed furnace, no preheat	18.6%		
Closed furnace, preheat	36.9%		



Table 2: Unit Process Input and Output Flows

Flow Name	Chromite concentrate from underground	Chromite concentrate from surface mining	Open furnace ferrochromium	Closed furnace, no preheat ferrochromium	Closed furnace, w/ preheat ferrochromium	Chromium metal	Units (Per Reference Flow)
Inputs							
Electricity [Electric power]	7.50E-02	8.30E-02	4.45E+00	4.42E+00	3.53E+00	1.61E-01	kWh
Water (municipal) [Water]	1.75E+00	1.20E+00	5.99E+00	3.42E+00	3.94E+00	3.78E+00	kg
Water (ground water) [Water]	1.22E+00	3.06E+00	5.29E+00	5.27E+00	5.84E+00	3.91E+00	kg
Water (surface water) [Water]	1.22E+00	3.06E+00	5.29E+00	5.27E+00	5.84E+00	3.91E+00	kg
Explosives [Operating materials]	5.00E-04	2.00E-03	1.10E-03	9.75E-04	1.02E-03	1.08E-03	kg
Diesel, combusted	2.70E-04	2.70E-04	7.06E-02	9.27E-04	3.05E-03	5.81E-04	kg
Heavy fuel oil, combusted	1.90E-04	1.90E-04	4.16E-04	3.71E-04	3.86E-04	4.09E-04	kg
Natural gas, combusted	2.10E-04	2.10E-04	4.60E-04	4.10E-04	4.26E-04	4.52E-04	kg
Liquid petroleum gas, combusted	1.20E-04	1.20E-04	2.63E-04	2.34E-04	2.44E-04	2.58E-04	kg
Light fuel oil, combusted	1.12E-03	1.11E-02	2.45E-03	2.18E-03	2.27E-03	2.41E-03	kg
Flocculant	1.30E-05	1.30E-05	2.85E-05	2.54E-05	2.64E-05	2.80E-05	kg
Coal	0.00E+00	0.00E+00	1.58E-01	2.10E-01	2.60E-02	0.00E+00	kg
Coke, imported	0.00E+00	0.00E+00	1.34E-01	1.91E-01	1.27E-01	0.00E+00	kg
Coke, local	0.00E+00	0.00E+00	1.30E-01	7.90E-02	1.72E-01	0.00E+00	kg
Char	0.00E+00	0.00E+00	1.10E-01	1.23E-01	2.45E-01	0.00E+00	kg
Anthracite	0.00E+00	0.00E+00	4.00E-02	9.10E-02	4.10E-02	0.00E+00	kg
Silica sand	0.00E+00	0.00E+00	2.20E-01	2.20E-01	2.20E-01	0.00E+00	kg
Electrode paste	0.00E+00	0.00E+00	1.50E-02	2.00E-02	1.00E-02	0.00E+00	kg
Thermal energy	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	5.41E+03	kJ
Soda ash	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	2.04E+00	kg
Sulfuric acid	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	9.43E-01	kg
Sulfur	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	3.08E-01	kg
Aluminum	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	5.19E-01	kg



Flow Name	Chromite concentrate from underground	Chromite concentrate from surface mining	Open furnace ferrochromium	Closed furnace, no preheat ferrochromium	Closed furnace, w/ preheat ferrochromium	Chromium metal	Units (Per Reference Flow)	
Outputs	Outputs							
chromite concentrate	1.00E+00	1.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	kg	
Ferrochromium	0.00E+00	0.00E+00	1.00E+00	1.00E+00	1.00E+00	0.00E+00	kg	
Chromium	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	1.00E+00	kg	
Tailings, from chromite beneficiation	6.80E-01	6.80E-01	1.49E+00	1.33E+00	1.38E+00	1.46E+00	kg	
FeCr slime	0.00E+00	0.00E+00	1.20E-01	1.10E-01	1.10E-01	0.00E+00	kg	
Slag	0.00E+00	0.00E+00	1.45E+00	1.58E+00	1.62E+00	0.00E+00	kg	
Iron (III) oxide	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	7.68E-01	kg	
Sodium sulfate	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	2.73E+00	kg	
Aluminum oxide	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	9.80E-01	kg	
Wastewater	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	1.73E-01	kg	
Carbon dioxide [Inorganic emissions to air]	0.00E+00	0.00E+00	1.53E+00	1.68E+00	1.51E+00	8.46E-01	kg	
Chromium (unspecified) [Heavy metals to fresh water]	1.10E-08	1.10E-08	2.41E-08	2.15E-08	2.23E-08	2.37E-08	kg	
Chromium (+III) [Heavy metals to air]	0.00E+00	0.00E+00	3.50E-04	0.00E+00	0.00E+00	0.00E+00	kg	
Chromium (+VI) [Heavy metals to air]	0.00E+00	0.00E+00	3.00E-07	0.00E+00	0.00E+00	0.00E+00	kg	
Lead [Heavy metals to air]	0.00E+00	0.00E+00	1.10E-06	1.10E-06	1.10E-06	0.00E+00	kg	
Manganese [Heavy metals to air]	0.00E+00	0.00E+00	1.50E-06	1.50E-06	1.50E-06	0.00E+00	kg	
Cadmium [Heavy metals to air]	0.00E+00	0.00E+00	1.40E-08	1.40E-08	1.40E-08	0.00E+00	kg	
Vanadium [Heavy metals to air]	0.00E+00	0.00E+00	7.60E-10	7.60E-10	7.60E-10	0.00E+00	kg	
Dust (unspecified) [Particles to air]	0.00E+00	0.00E+00	3.80E-03	4.80E-03	4.80E-03	0.00E+00	kg	
Zinc [Heavy metals to air]	0.00E+00	0.00E+00	0.00E+00	0.00E+00	1.10E-03	0.00E+00	kg	

^{*} Bold face clarifies that the value shown does not include upstream environmental flows.

Embedded Unit Processes

None.

References

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Section III: Document Control Information

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